

AMENDMENTS TO THE CLAIMS

Please amend claims 31 and 32 as shown below.

1. (Previously Presented) A solvent extraction mixture for extracting oil from an oil bearing material, the solvent extraction mixture comprising:
oil bearing material that presents a combination of triglyceride oil and phospholipid oil for extraction; and
a solvent at a temperature ranging from 35°C to 55°C, the solvent having a viscosity ranging from 0.3 to 2.6 centipoise and a polarity index no greater than about 0, the solvent containing
 - (a) a low molecular weight hydrocarbon constituent ; and,
 - (b) a halocarbon constituent selected from the group consisting of fluorocarbon, chlorocarbon, and chloroflouorocarbon materials in an effective amount to provide selective extraction of the triglyceride oil in preference to the phospholipid oil, as compared to extraction using the hydrocarbon constituent.
2. (Previously Presented) The solvent extraction mixture of claim 1 wherein the hydrocarbon constituent is of a formula $C_nH_{(2n+2)}$ or C_nH_{2n} with n equal to between 5 and 8.
3. (Previously Presented) The solvent extraction mixture of claim 2 wherein the hydrocarbon constituent is a hexane.
4. (Previously Presented) The solvent extraction mixture of claim 1 wherein said the halocarbon constituent is selected as the fluorocarbon having a polarity index of less than 0.1.
5. (Previously Presented) The solvent extraction mixture of claim 4 wherein said the fluorocarbon has a polarity index ranging between about - 2.0 and about 0.1 and a dielectric constant ranging between about 1.7 and about 2.0.
6. (Cancelled)
7. (Cancelled)
8. (Cancelled)
9. (Previously Presented) The solvent extraction mixture of claim 3 wherein the hexane is selected from the group consisting of straight-chained hexanes, branch-chained hexanes, and mixtures thereof.

10. (Previously Presented) The solvent extraction mixture of claim 1 wherein ~~said~~ the halocarbon constituent is selected as the fluorocarbon further selected from the group consisting of $C_nH_{(2n+2)-x}F_x$, where n equals between 4-8 and x equals between 1-17; $C_nF_{(2n+2)}$, where n equals between 5-8; $C_nCl_{(2n+2)-x}F_x$, where n equals between 1-6 and x equals between 1-13; $C_nH_{(2n+2)-(x+f)}Cl_xF_f$, where n equals between 1-4, x equals between 1-9, and f equals between 1-9; and, $C_nH_{(2n+2)-x}Cl_x$, where n equals between 1-4, and x equals between 1-9.

11. (Previously Presented) The solvent extraction mixture of claim 10 wherein the fluorocarbon is selected from the group consisting of $C_5H_2F_{10}$, C_6HF_{13} , C_7HF_{15} , $C_{10}HF_{21}$, C_5F_{12} , C_7F_{16} , C_6F_{14} , C_8F_{18} , $C_2Cl_3F_3$, CCl_3F , $C_3Cl_2F_6$, $C_4Cl_2F_8$, $C_4Cl_3F_7$, C_6ClF_{13} , $C_3HCl_2F_5$, and $C_2HCl_2F_3$.

12. (Previously Presented) The solvent extraction mixture of claim 1 wherein the halocarbon constituent is selected as the fluorocarbon further selected from the group consisting of hydrofluorocarbon, perfluorocarbon, hydrochlorofluorocarbon, and combinations thereof.

13. (Previously Presented) The solvent extraction mixture of claim 1 wherein the halocarbon constituent is selected as the fluorocarbon is being a hydrofluorocarbon.

14. (Previously Presented) The solvent extraction mixture of claim 1 wherein the halocarbon constituent is selected as the ~~said~~ fluorocarbon and the effective amount ranges between 60% and 70% by volume of the solvent.

15. (Cancelled)

16. (Previously Presented) A solvent extraction mixture for extracting oil from an oil bearing material, the solvent extraction mixture comprising:

oil-bearing material-that presents a combination of triglyceride oil and phospholipid oil for extraction; and

a solvent at a temperature ranging from 35°C to 55°C, the solvent having a viscosity ranging from 0.3 to 2.6 centipoise and a polarity index no greater than about 0, the solvent containing

(a) a low molecular weight hydrocarbon constituent ; and,

(b) a halocarbon constituent in an effective amount to provide selective extraction of the triglyceride oil in preference to the phospholipid oil, as compared to extraction using the hydrocarbon constituent alone.

17 -30 (Cancelled)

31. (Currently Amended) A solvent mixture for extracting oil from ~~an~~ a soybean oil bearing material so as to form an extracted oil comprised of greater than 95% by weight triglycerides and other non-polar constituents, with said solvent having a polarity no greater than about 0 and a viscosity ranging between about 0.3 centipoise and about 2.6 centipoise, whereby the triglycerides are miscible in said solvent at a temperature ranging between about 35° C and about 55° C and after extraction of the triglycerides said solvent and the triglycerides form a miscella, and at a temperature ranging between about 15 ° C and about 25 ° C, said miscella will form distinct solvent and oil layers that can be separated, said solvent mixture comprising:

- (a) an amount of a low molecular weight hydrocarbon having a viscosity of less than 2.6 centipoise; ~~and,~~
- (b) a fluorocarbon solvent or a chlorocarbon solvent wherein said chlorocarbon is selected from the group consisting of CH₂Cl₂, C₂H₃Cl₃, and C₂HCl₃;

and wherein said fluorocarbon solvent is selected from the group consisting of

C₅H₂F₁₀, C₆HF₁₃, C₇HF₁₅, C₁₀HF₂₁, C₅F₁₂, C₇F₁₆, C₈F₁₈, C₂Cl₃F₃, CCl₃F, C₃Cl₂F₆, C₄Cl₂F₈, C₄Cl₃F₇, and C₆ClF₁₃; and

soybean material that presents a combination of triglyceride oil and phospholipid oil for extraction,

the low molecular weight hydrocarbon constituent and the fluorocarbon solvent being present in effective amounts for selectively extracting the triglyceride oil while leaving the phospholipid oil in the soybean material, such that crude oil to be extracted from the soybean oil bearing material has a phospholipid content of less than 0.1% by weight.

32. (Currently Amended) A solvent mixture for extracting oil from ~~an~~ a soybean oil bearing material so as to form an extracted oil comprised of greater than 95% by weight non-polar constituents, with said solvent having a polarity no greater than about 0 and a viscosity less than about 2.6 centipoise, whereby the non-polar constituents are miscible in said solvent at a temperature ranging between about 35° C and about 55° C and after extraction of the non-polar constituents, said solvent and the non-polar constituents separate

at a temperature ranging between about 15 ° C and about 25 ° C, forming distinct solvent and oil layers that can be separated, said solvent mixture comprising:

- (a) an amount of a low molecular weight hydrocarbon; ~~and,~~
- (b) a non-polar halogenated solvent;

wherein said non-polar halogenated solvent is selected from the group consisting of CH₂Cl₂, C₂H₃Cl₃, C₂HCl₃, C₅H₂F₁₀, C₆HF₁₃, C₇HF₁₅, C₁₀HF₂₁, C₅F₁₂, C₇F₁₆, C₈F₁₈, C₂Cl₃F₃, CCl₃F, C₃Cl₂F₆, C₄Cl₂F₈, C₄Cl₃F₇, and C₆ClF₁₃; and

soybean material that presents a combination of triglyceride oil and phospholipid oil for extraction,

the low molecular weight hydrocarbon and the non-polar halogenated solvent being present in effective amounts for selectively extracting the triglyceride oil while leaving the phospholipid oil in the soybean material, such that crude oil to extracted from the soybean oil bearing material has a phospholipid content of less than 0.1% by weight.